

METHOD OF CO-CRYSTALLIZING A FOOD ADDITIVE

- The present invention relates to the preparation of food additives, in particular to the preparation of flavours for incorporation into foodstuffs, as well as to the additives and foodstuffs, particularly animal feeds, obtained thereby.
- Many foodstuffs for both human and animal consumption are processed for the incorporation of additives. With respect to animal feeds, a clear relationship between food flavour and feed intake has been recognised.
- Hitherto, flavour compounds have been incorporated into foodstuffs, particularly animal feeds, by addition to carrier particles, in particular, salt particles. The flavour compounds in liquid or powder form are distributed onto fine salt particles which may then be added to foodstuffs. The particle size of the salt particles used as a carrier is necessarily small in order to ensure that the surface area of the carrier onto which the flavour may be adsorbed, is as large as possible so as to optimise the amount of flavour to the amount of carrier. The problem here is that the final product is dusty, being only of a similar size to the fine salt particles utilised as the carrier. Significant quantities of dust in the atmosphere is undesirable, particularly in industrial environments since small particles present in the air, may be breathed in by workers in the area, and may adversely affect health.

Furthermore, being merely coated on the surface of the carrier particles, the flavour compounds may be relatively easily and rapidly lost, for example, by abrasion and/or

vapourisation leading to a reduced shelf life or persistence of flavour of both the additive and the finished product (foodstuff).

- 5 The applicants have found an improved method of formulating food additives, which produces a more easily handled and robust product.

According to the present invention, there is provided a
10 method of preparing a food additive, said method comprising

(i) mixing crystalline carrier particles with an additive compound;

(ii) applying to the thus produced mixture a solution of a crystalline solid under conditions such that the said
15 carrier particles are partially dissolved; and

(iii) allowing the mixture to cocrystallize and to agglomerate so as to form particles of increased average size as compared to the said carrier particles.

- 20 During the cocrystallization step (iii), the particles grow and/or coalesce. Thus the average particle size of the product is generally larger than the particle size of the carrier molecules themselves. Such particles will present a reduced dust hazard as compared to the carrier particles
25 themselves.

Furthermore, during the cocrystallisation in step (iii), the additive becomes incorporated into pores in the resultant crystal structure. The crystals are, by and large, coated
30 with the crystalline solid, so that the additive is entrapped within the larger particles. This means that the additive is not easily lost or degraded by other components in the foodstuff. Therefore, the shelf life of the food

additive, as well as the feed or food product incorporating the additive, is also increased.

Suitable carrier particles are non-toxic crystalline solids such as salt or sugar crystals. In particular alkali metal halides in particular chlorides such as sodium or potassium chlorides are preferred carrier particles. Such compounds are economical and readily available and are generally permitted in animal feeds.

10

The carrier particles may comprise a mixture of the carriers and also dessicating or drying agents as 'co-carriers'.

These agents include edible silica and silicates, for example Sipername® 22 available from Degussa. These agents can absorb up to 2.5 times their own weight of moisture. Inclusion of such agents may be preferable where the additive compound is in the form of a liquid (either a liquid *per se* or a solution such as an aqueous solution), likely to form a 'sticky' product when combined with the carrier. The amount of such a co-carrier required will depend upon the amount of additive compound as well as the precise nature of the additive compound and the carrier. In general, the weight ratio of co-carrier to liquid additive compound would be in the region of about 1:2 so that if 20 g of liquid additive were to be used, the carrier would include 10g of co-carrier.

Preferably the carrier particles have an average particle size of from 50-300 microns, and are generally in the region of about 200 microns.

Examples of food additives which may be incorporated in this way include flavours, vitamins in particular vitamin E or vitamin A or other diet supplements, preservatives,

colorants, etc. The additives are suitably in the form of liquids or solids at room temperature. The method is particularly suitable for the inclusion of flavours for example natural flavours such as vanilla or flavour

5 composites containing such as Butter Vanil Arome Dry® (available from Kemin Europa N.V.), as well as artificial flavours such as pyrazines, esters and ketone flavours as would be understood in the art.

10 The ratio of the food additive to carrier particle which are mixed together in step (i) depends upon the precise nature of the carrier particles and the additive compounds employed. However, a weight ratio of carrier (including co-carrier where present) to additive of from 1:1 to 99:1, 15 suitably about 4:1 will generally be acceptable.

The solution utilised in step (ii) of the process of the invention is suitably an aqueous solution of a material which forms a non-toxic crystalline solid at room

20 temperature. The solid preferably has a palatable flavour of its own, so that it may enhance the flavour of the additive. Examples of such compounds are sugars, such as glucose, maltose or fructose or other sweeteners. Such compounds are readily available and low in cost which is 25 particularly important for animal feed applications.

The solution of crystalline solid used in step (ii) is suitably a concentrated aqueous solution, containing for example of from 30-65wt%, preferably about 40wt% crystalline 30 solid. This is particularly true for sugar solutions where concentrations in excess of 65wt% are regarded as being syrups.

The solution must be applied in such a way that it results in only partial dissolution of the carrier particles. The conditions under which this will happen depends upon the precise nature of the carrier particles as well as the 5 nature of the solution of crystalline solid. A preferred application method is by spraying the solution onto the particles, and thus it is preferable that the solution is able to pass through a nozzle of a spray applicator, most preferably a fine nozzle of from 0.46mm to 0.97mm in size.

10 A flow rate of from 0.28 l/min to 0.84 l/minute, suitably at about 0.56 l/minute may be utilised.

When applied in this way, the spray droplets of the water/sugar solution wet the contact surface of the salt 15 containing the additive, such as flavour, components. As a result, co-crystallisation of the sugar and the outer layer of the salt occurs, together with coating of the contact area with the liquid sugar solution. The additive, such as the flavour, becomes stably incorporated into the particles 20 thus formed.

The solution may optionally include other active components such as flavour enhancers for example maltol or heliotropine, artificial sweeteners such as saccharine, or 25 fixatives.

Conditions under which the solution of crystalline solid is applied in step (ii) will vary depending upon the precise nature of the carrier molecules, the additive, the 30 crystalline solid itself as well as the process equipment employed. However temperatures of from 10°C to 50°C, suitably at about 25°C may be used.

The amount of solution applied to the carrier/additive mixture to achieve the desired product will once again depend upon the precise nature of the components and the process equipment. However, in general, the amount of 5 solution applied will be of the order of from 5 to 25wt% of the amount of the additive in the mixture, suitably at about 10% by weight.

10 The cocrystallisation and agglomeration of step (iii) of the process of the invention may occur or begin to occur during the spraying step (ii) depending upon the particular conditions employed. After spraying, the sprayed product is subjected to conditions which would allow co-crystallisation and agglomeration of the components to occur or to continue, 15 as necessary. This may include maintaining the product at moderate temperatures for example of from 15° to 50°C, optionally in a moving air stream for example as may be found in a fluidised dryer.

20 Once prepared in this way, the product is generally quite dry but optionally may be subjected to extra drying. This can be accomplished using a fluid bed dryer with an air temperature of from about 60 to 150°C, suitably at about 100°C and a product temperature of about 25°C. Drying times 25 may be relatively short, for example from 2 to 20 minutes.

The resultant particles generally have an particle size in excess of 300 microns, for example about 500 microns.

30 Thus the invention further provides a particulate food additive comprising a non-toxic soluble salt, a food additive and a sugar which have been subjected to co-crystallization.

Such food additive particles can be admixed with foodstuffs and in particular animal feeds in a conventional manner. The size of the particles means that the handling process 5 can be carried out more easily and with less dust than hitherto.

In yet a further aspect, there is provided a foodstuff comprising a particulate food additive as described above.

10

Another aspect of the invention provides a method for supplementing a foodstuff, said method comprising mixing said foodstuff with a particulate food additive in the form of a particulate material as described above.

15

The invention will now be particularly described by way of example.

Example 1

20 Butter Vanille Arome Dry flavour [®](250g) from Kemin Europa N.V. contains vanilla on a carrier comprising sodium chloride (74wt%) with a silicate as a co-carrier (10wt%). This product has an average particle size of 0.2mm.

25 A sugar solution (300g sugar in 750ml water) was prepared.

26 g of the sugar solution was applied to the Butter Vanille Arome Dry[®] by spraying.

30 The resultant crystalline product was transferred to a fluid bed dryer and dried with an air temperature of 100°C and a product temperature of 30°C for five minutes.

The resultant product was in the form of uniform rounded granules having an average particle size of 0.5mm.